

# Simulation of Coal Particles in a Full Chemical Looping Combustion System

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## **Objectives**

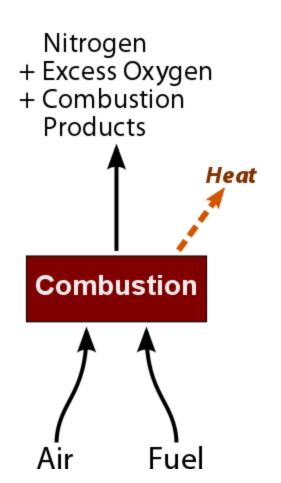
- Develop a Chemical Looping Combustion model
  - Full loop, 3D geometry
  - Fluid-particle dynamics
  - Oxidation/reduction chemistry
  - Coal devolatilization, moisture release, gasification reactions
  - Thermal characteristics

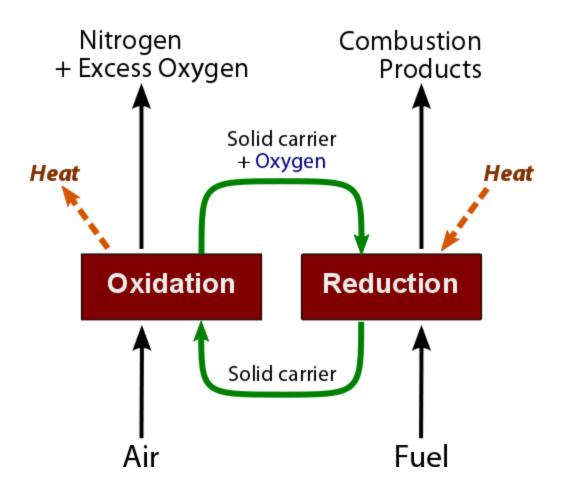




#### **Traditional Combustion**

#### **Chemical Looping Combustion**

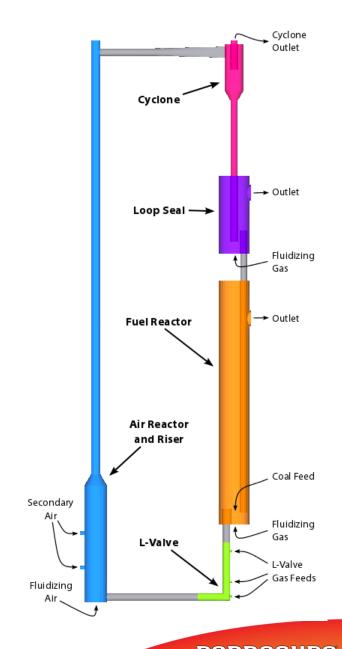






## Model geometry

- Design provided by NETL for 800 lb/hr circulation of solids carrier
- Approximately 12' tall
- Geometry contains equipment for reactions
  - Air reactor
  - Fuel reactor
- Solids circulation and separation
  - Cyclone
  - Loop seal
  - L-valve

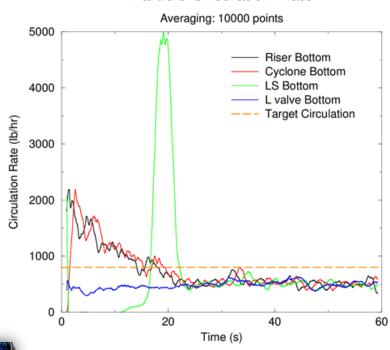


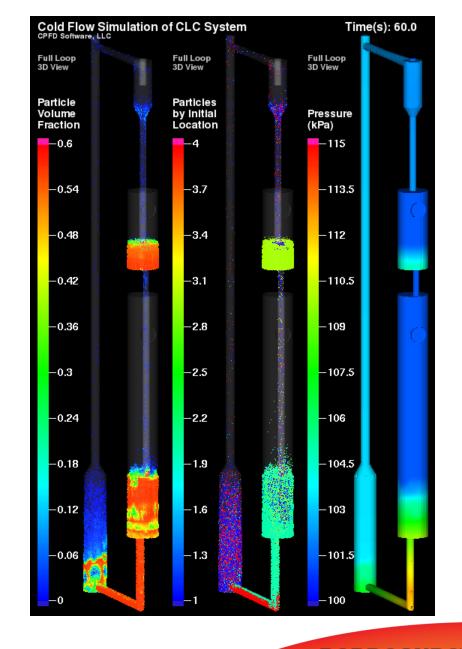


### Cold flow model

- Isothermal at 298K
- Non-reacting

#### Particle Circulation Rate









## **Modeling CLC Reactions**

- Key features
  - Multicomponent particles
  - Particle level chemistry
- Multicomponent particles provide Lagrangian tracking of particle composition
- Particle level chemistry provides a separate domain to each computational particle for reaction calculations
  - Particle composition
  - Particle temperature
  - Particle diameter, area, etc
  - Fluid properties

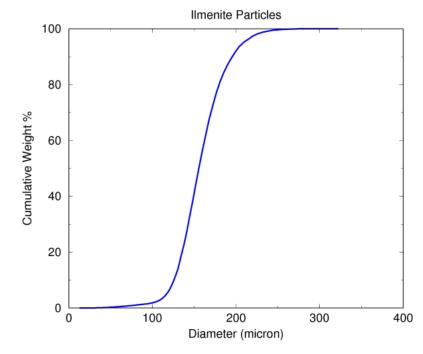




#### **Ilmenite Carrier**

- Primarily consists of
  - ilmenite (FeTiO<sub>3</sub>)
  - rutile (TiO<sub>2</sub>)
  - hematite (Fe<sub>2</sub>O<sub>3</sub>)
- d<sub>50</sub> of 156 microns
- Oxygen carrying capacity:
  3.3 wt% of oxidized particle weight

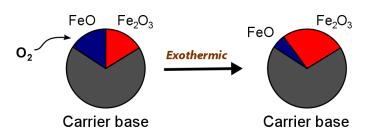
#### Particle Size Distribution





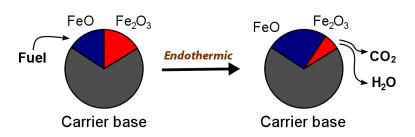
## Ilmenite chemistry

#### Oxidation (exothermic)



$$4\text{FeO} + \text{O}_2 \rightarrow 2\text{Fe}_2\text{O}_3$$

#### Reduction (endothermic)



$$4\text{Fe}_2\text{O}_3 + \text{CH}_4 \rightarrow 8\text{FeO} + \text{CO}_2 + 2\text{H}_2\text{O}$$

$$Fe_2O_3 + H_2 \rightarrow 2FeO + H_2O$$

$$Fe_2O_3 + CO \rightarrow 2FeO + CO_2$$







#### **CLC** subset models

- Apply ilmenite chemistry
  - air reactor subset model
  - fuel reactor subset models



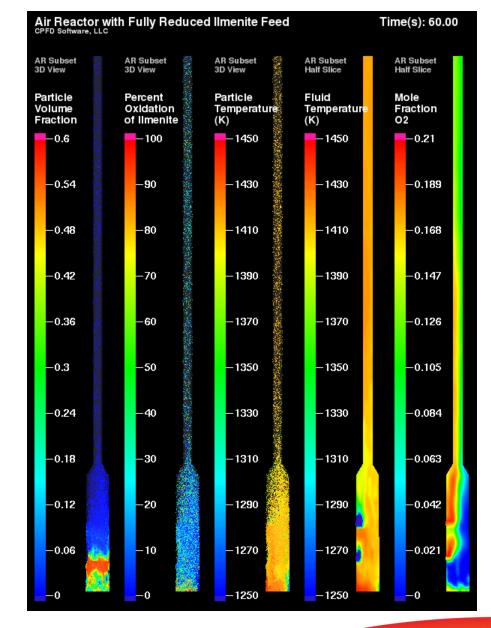


### Air reactor subset

Ilmenite enters air reactor completely reduced

Percent Oxidation = 
$$\frac{w_{\text{Fe}_2\text{O}_3}}{0.307} \times 100$$

 Max Fe<sub>2</sub>O<sub>3</sub> on particle: 30.7 wt%

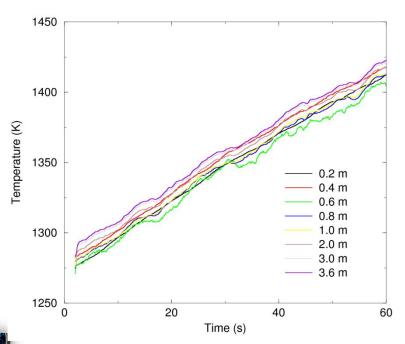




## Oxidation level of ilmenite feed

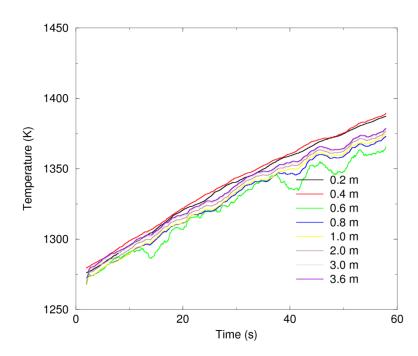
 Ilmenite enters air reactor unoxidized

Temperatures in Air Reactor



Ilmenite enters air reactor
 65% oxidized

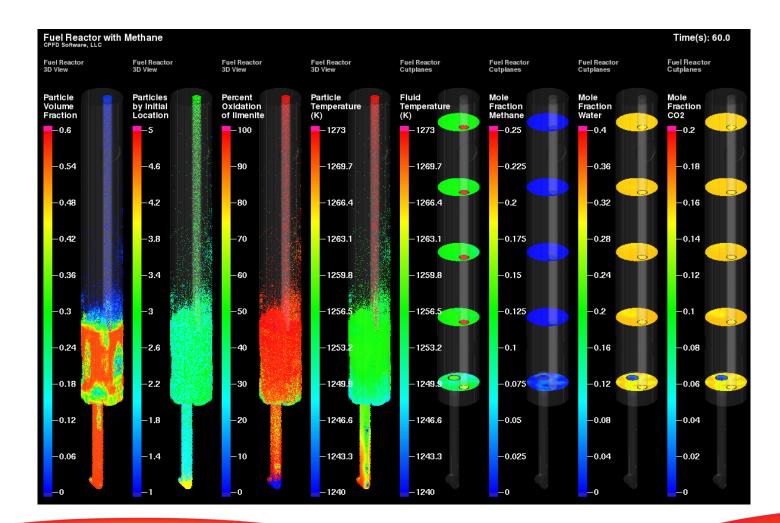
Temperatures in Air Reactor







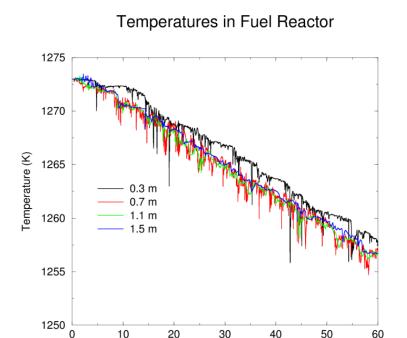
#### Fuel reactor subset with methane

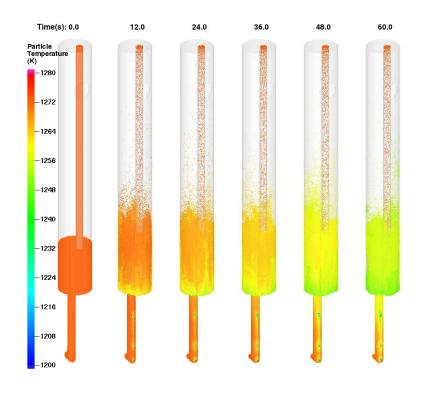






## Temperatures in Fuel Reactor with methane









Time (s)

## **Coal chemistry**

#### Coal devolatilization

- Temperature-dependent release of <u>methane</u>, <u>carbon dioxide</u>, <u>carbon monoxide</u>, <u>water</u>
- Included particle swelling effects

#### Coal drying

 Mass transfer limited release of moisture from particle. Equilibrium between solid and gas phase.

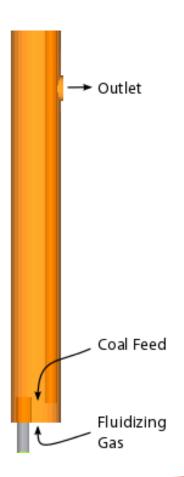
#### Gasification of carbon

- Steam gasification producing <u>carbon monoxide</u>, <u>hydrogen</u>
- CO<sub>2</sub> gasification producing <u>carbon monoxide</u>

#### Water-gas shift reaction

#### Ilmenite reduction reactions

Reduction reactions of <u>Methane</u>, <u>Hydrogen</u>, <u>Carbon monoxide</u>





## **Coal particle properties**

 Initial particle density: 1333 kg/m<sup>3</sup>

- 50 micron 150 micron particle diameter
- Heat of combustion: 32 MJ/kg

#### <u>Initial coal composition</u>

Component	Composition (wt%)	Density (kg/m³)
Char	51%	2150
<b>Volatile Organics</b>	34%	815
Ash	10%	2200
Moisture	5%	1000

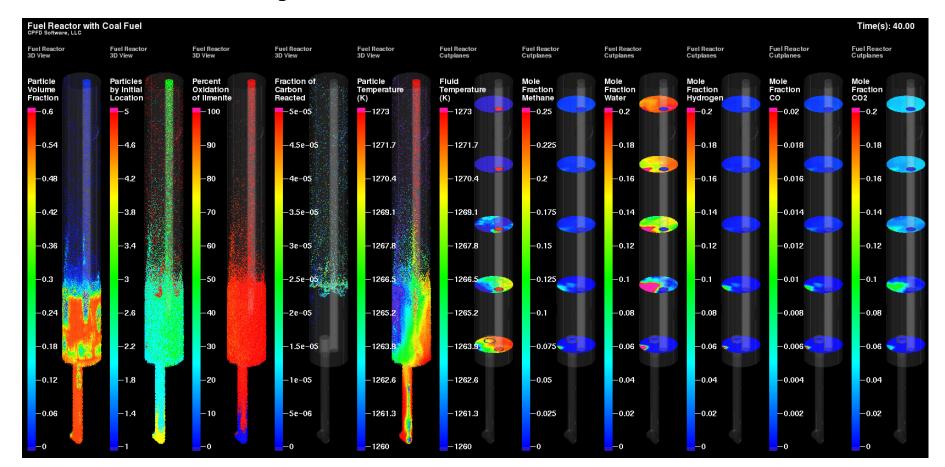
#### **Released Gases**

Component	Composition (wt%)
Methane	66.8%
Carbon monoxide	24.4%
Water	5.9%
Carbon dioxide (gas)	2.8223%
Carbon dioxide (trapped)	0.0777%





## Coal particle subset model



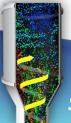




### **Full CLC simulation with coal**

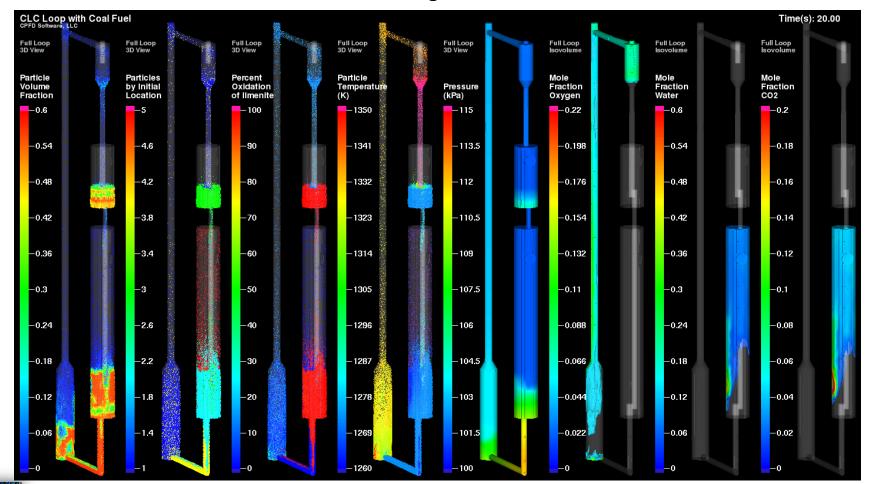
Apply ilmenite chemistry and coal chemistry to loop

Coal feed is 2.7 lb/hr at 298K





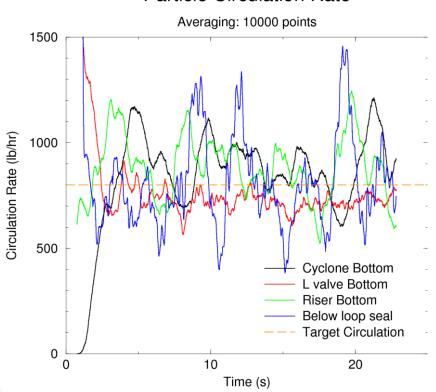
## **Full CLC loop simulation**





## **Full CLC loop simulation**

#### Particle Circulation Rate



 Simulated circulation rate is close to target rate of 800 lb/hr





#### **Conclusions**

- Full reacting chemical looping combustion system was modeled in 3D
- Model highlights
  - Composition of solid ilmenite carrier was tracked on each computational particle in model
  - Oxidation/reduction of ilmenite is modeled using particle level chemistry
  - Coal particles were modeled as a fuel source, including devolatilization, moisture release, and gasification reactions
- Tool for future design and optimization work





## Acknowledgements

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